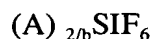


MARKED UP VERSION OF AMENDED CLAIMS

1. (Once Amended) A [P] process for the catalytic dewaxing of a hydrocarbon oil feed including waxy molecules and more than 500 ppmw of sulphur or sulphur containing compounds by contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.
2. (Once Amended) The [P] process [according to] of claim 1, wherein the oil feed comprises more than 750 ppmw of sulphur or sulphur containing compounds.
3. (Once Amended) The [P] process [according to any one of claims 1-2,] of claim 1, [wherein] in which the oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.
4. (Once Amended) The [P] process [according to any one of claims 1-3,] of claim 1, [wherein] in which the hydrogenation component is platinum[, palladium or nickel].
5. (Once Amended) The [P] process [according to any one of claims 1-4,] of claim 1, [wherein] in which the low acidity binder is silica.
6. (Once Amended) The [P] process [according to any one of claims 1-5,] of claim 1, [wherein] in which the aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.
7. (Once Amended) The [P] process [according to] of claim 6, [wherein] in which the aluminosilicate zeolite crystallites is of the MFI type.

8. (Once Amended) The [P] process [according to any one of claims 1-7,] of claim 1, [wherein] in which the dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:



[wherein] in which 'A' is a metallic or non-metallic cation other than H+ having the valence 'b'[, preferably ammonium].

9. (Once Amended) The [P] process [according to any one] of claim[s] 8, [wherein] in which an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.

10. (Once Amended) The [P] process [according to any one of claims 1-9] of claim 1, [wherein] in which the oil feed is a solvent extracted waxy raffinate.

11. (Once Amended) The [P] process [according to any one of claims 1-9] of claim 1, [wherein] in which the oil feed is a gas oil.

12. (Once Amended) The [P] process [according to any one of claims 1-9] of claim 1, [wherein] in which the oil feed is a hydrocracker feedstock and wherein the dewaxed oil is subsequently subjected to a hydrotreating step before being subjected to a hydrocracker process step in which step primarily middle distillates are prepared.

13. (Once Amended) A method of [Method for] retrofitting a process for preparing lubricating base oils [wherein] in which an existing solvent dewaxing step is replaced by a catalytic dewaxing process comprising the steps of contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina [according to any one] of [claims 1 to 10.] claim 1.

Please add new claims 14, 15 and 16:

14. The process of claim 8, where 'b' is ammonium.

15. The process of claim 1, in which the hydrogenation component is palladium.

16. The process of claim 1, in which the hydrogenation component is nickel.